# **USING METHYL UREA AS INHIBITOR FOR THE CORROSION OF CARBON STEEL IN 1M HYDROCHLORIC ACID MEDIUM**

#### **Dunya Edan Al-Mammar**

*Department of Chemistry, College of Science, University of Baghdad. Baghdad- Iraq* 

#### **Abstract**

 The corrosion behaviour of carbon steel in 1M HCl solution containing various concentration of methyl urea range  $(10^{-3} \rightarrow 5 \times 10^{-2})$ M at temperature range (285-313)K was investigated. The corrosion inhibitive action of methyl urea on carbon steel was studied using weight loss measurement and atomic absorption analysis to find the amounts of dissolved metal in acidic solution in presence and absence of methyl urea. The results showed that urea caused protection efficiency reached to 82% when  $(10^{-3})$ M methyl urea concentration was used. The coverage ( $\theta$ ) of metal surface by methyl urea could be obtained from the rate of corrosion in the presence and absence of methyl urea in the acid solution. Results obtained by gravimetric and atomic absorption are in good agreement. A linear relationship was found to exist between the value of  $(C/\theta)$  and the corresponding methyl urea concentration  $(C)$ indicating that the inhibition action occurs via adsorption mechanism. Changes in the free energy, enthalpy and entropy associated with methyl urea adsorption have been determined. Apparent energies of activation have been calculated for the corrosion process of iron in the acid from corrosion rates and Arrhenius plots.

#### **الخالصة**

 تم دراسة السلوك التاكلي للحديد الكربوني في محلول 1 مولاري من حامض الهيدروكلوريك علـى مـدى مـن التراكيز المختلفة في مثيل يوريا كمثبط للتأكل تراوحت بين (10-2-10-35 (مولاري بمدى من درجات الحرارة تراوحـت بـين (313-285) كلفـن. وتمـت هـذه الدراسـة باسـتخدام تقنيتـين مختلفتـين همـا -1تقـدير الـوزن المفقـود للحديد الكربوني نتيجة التأكل، 2– تقدير الحديد الذائب في محلول الحامض بطريقة الامتصاص الذري وبوجود وغياب المثيل يوريا في المحلول كمثبط.

 وقـد اظهـرت النتـائج ان المثيـل يوريـا خفـضت عمليـة التأكـل الـى 82 % عنـد تركيـز 10-3 مـولاري وامكـن ايجاد مقـدار تغطيـة ( (سـطح النمـاذج بالمثيـل يوريـا مـن حـساب سـرعة التأكـل بوجـود وغيـاب المثيـل يوريـا فـي الوسط الحامـضي. وتبـين ان هنـاك تقـارب بـين القـيم المستحـصلة بـالطرق الوزنيـة والطيفيـة وقـد اظهـرت الدراسـة وجود علاقـة خطيـة بـين قيم (C/θ) وتراكيـز (C) للمثيل يوريـا المنـاظرة لـهـا موضـحاً حدوث فعل التثبيط من خـلال عمليـة الامتـزاز. وتـم دراسـة التغيـر فـي قيمـة الطاقـة الحـرة والانثـالبي والانتروبـي المرافقـة لامتـزاز المثيـل يوريـا علـى سـطح المعـدن وتـم ايجـاد طاقـة التنـشيط لعمليـة التأكـل وذلـك مـن قياسـات سـرع التأكـل فـي الـدرجات الحرارية المختلفة وعلاقة ارينيوس.

#### **Introduction**

 The dissolution behavior of carbon steel in acidic and nearly neutral media was known to be inhibited by nitrogen and sulfur containing organic compounds[1-2].

Such compounds contain electron-donating groups that decrease the corrosion rate by increasing the hydrogen overvoltage on the corroding metal [3].

The use of nitrogen containing compounds as corrosion inhibitors is widespread. These compounds can bind to metal surfaces by electron transfer to form a coordinated bond and hence iron effective inhibition [4].

Polarization measurements on the organic compounds indicate that they are cathodic inhibitors[5]. Methods of comparing the inhibition efficiencies of surfactants are numerous and involve, among others, weight loss determination, electrode potential measurements, construction of electrocapillary curves depression of polarographis maxima, determination of electrode reaction parameters and determination of elements dissolved by ultraviolet-visible absorption spectroscopy[6]. The corrosion inhibition of carbon steel have been observed potentiostatically by many workers[7], however, most of the interests of these workers mainly were related to the effect of the type of functional groups of the organic inhibitors and the best percentage of inorganic compounds to each complete protection.

The inhibiting action of some urea compound on the corrosion behavior of (410) steel in 1M  $H_2SO_4$  was understood using weight loss measurements, the adsorption followed the langmuir adsorption isotherm.

The best protective properties from sols consisting of three  $SiO<sub>2</sub>$  layers with nanosilica and three  $SiO<sub>2</sub>$  layers without nanosilica [8].

The kinetics and thermodynamics of the corrosion process and the actual role of certain chemicals in corrosion inhibition are among the aspects which attrarted relatively little attention.

In the present work has therefore been planned to investigate the weak corrosion behaviour of carbon steel specimen in 1M HCl. The research also involved the use of methyl urea as an inhibitor for the acid corrosion of carbon steel. The effect of the inhibitor on the corrosion rate has been estimated using both weight loss and atomic absorption spectroscopy measurement. Inhibitors are widely used to control the corrosion of metallic materials and function one or more of the following mechanisms [9]:

1- by adsorption on the surface of according material.

2- by changing the corrosion characteristics of the environment.

3- by inducing the function of a protective layer of corrosion product.

### **Experimental**

 Low carbon steel AISI 5135 (obtained from ministry of industry) had the following

composition as revealed by emission spectroscopic analysis:-

Element					
	0.38	$\left  0.035 \right  0.035 \left  \begin{array}{c} 0.15 \\ 0.35 \end{array} \right  0.5 - \left  \begin{array}{c} 0.9 \\ 1.2 \end{array} \right $			
wt. %					

were used for the measurement of the corrosion rate. All test spieces having thickness about 7mm and diameter 17 mm.

Specimens were abraded in sequence under run tap water by using the following emery paper grades; 220, 320, 400 and 600, washed with run tap water followed by distilled water, dried with cotton, immersed in ethyl alcohol and dried, immersed in acetone, they were left to dry over silica gel before use.

Each experiment was carried out with 20ml of the corroding solution and with fresh test piece. The temperature was measured to  $(\pm 0.1)^{\circ}C$ . All chemical were used of A.R. quality and were employed without further purification. 1M hydrochloric acid solution was prepared by analytical dilution from stock solution.

After each test, specimens were washed with running tap water, cleaned with brush to remove the weakly with adherent corrosion scale, rinsed with distilled water, swabbed with cotton wool soaked in  $5\%$  H<sub>2</sub>SO<sub>4</sub> containing 0.011 wt.% thiourea [10] to remove all adherent corrosion products. Then specimens were washed with tap water followed by distilled water and dried.

Then the specimen were rinsed with analar benzene, dried with Klennex tissue followed by rinsing with analar acetone, dried with Kleenex tissue, then left to dry and weighed to the  $4<sup>th</sup>$ decimal of gram. In order to analyse elements dissolved in 50 solutions after weight loss tests, atomic absorption spectroscopy was used with acetylene-air flame, and the wavelengths were employed was  $2483A^{\circ}$  for Fe.

### **Results**

## **Weight Loss Measurements**

 The corrosion of carbon steel in 1M HCl solution containing various methyl urea concentration studied by weight loss measurements at various temperature (285- 313)K at immersion period of 2h. The corrosion rate of carbon steel is determined by using the relation.

 $R_{(w) \text{ loss}} = \Delta m / \Delta t$  ……...(1) mg.cm<sup>-2</sup>.hour<sup>-1</sup>  $\mathbf{R}_{(w) \text{A-A}} = \Delta \mathbf{m}/\Delta t$  …….(2)

Where  $\Delta m$  is the mass loss of the metal in the acidic solution and  $\Delta t$  is the immersion period. The corrosion rate result is shown in Table (1).

## **Corrosion Protection**

 The percentage protection efficiency %P is calculated using the relationship [11]:

 $\%P=((1-R_{\text{winh}})/R_{\text{wo}})\times 100$  ………(3)

Where  $R_{(with)}$ ,  $R_{wo}$  are the corrosion rate of carbon steel in presence and absence of methyl urea. Table (2) shows the percent protection efficiency (P%) using the weight loss and atomic absorption measurements. The protection efficiency increase with temperature increase at low concentration of methyl urea as shown in Figure (1a,b).

There was an initial sharp increasing in P% Figure. (2a) subsequent to the first additions of the inhibitor (1.0 to 10 mM) remaining there after constant over concentration from (25 to 50 mM).

P% values were plotted at different methyl urea concentrations (Figure2a,b) and were found dependent of temperature.

The temperature effect was significant in the presence of high concentration of methyl urea and P% increased with temperature increasing. This result may be interpreted by many authors<sup> $(5)$ </sup> for the following reasons: temperature is a predominant factor in the formation of a protective layer at the metallic surface formed by metal inhibitor interaction.

The P% calculated from weight loss and atomic absorption measurements varied with methyl urea concentration at temperature varing (285- 313)K Figure (2 a,b).

## **Adsorption and Surface Coverage**

The degree of coverage  $\theta_{inh}$  of the carbon steel surface by methyl urea could be calculated using the equation:

 $\hat{\theta}_{inh}=(R_{(wo)}-R_{(winh)})/R_{wo}$  ………...(4)

The  $\theta_{inh}$  values shown in Table (2). The maximum values of  $\theta$  at 313K (0.7169) but were relatively lower at 307K (0.16633).

The adsorption behavior of methyl urea on carbon steel surface, can be described as indicated in Figure(3 a,b) where linear relationship is shown to exist between the values of  $(C/\theta)$  and the corresponding urea concentration (C). Such relationships suggest that methyl urea acts as corrosion inhibitor via

adsorption on carbon steel surface. The type of adsorbate-adsorbent interaction follows langmuir adsorption isotherm which may be represented as [12]:

$$
C/\theta = (1/b) + C \dots \dots \dots (5)
$$

Where (1/b) is the intercept of each line on the  $(C/\theta)$  axis when methyl urea concentration  $(C)$ approaches zero. The constant b in equation (5) may be considered as an equilibrium constant which could be defined by the following equation $^{(13)}$ :

**b = a exp (q/RT) ………(6)** 

Where q is the heat of methyl urea adsorption on carbon steel surface.

The per-exponential factor (a) in equation (6) includes several other terms [14] relating to condensation and adsorption processes. The values of b which have been derived from the intercepts of the plots in Figure(4) are described in Table (3).

Thus there is a smoth increase in the values of b with the rise of temperature from  $(285-313)$ K.

A plot of log b against (1/T) (equation.6) should produce a straight line provided (q) and (a) remained independent of temperature as indicated in Figure.(4). The heats of adsorption derived from the slopes of two lines were respectively  $23.159$  and  $12.472 \text{kJ/mol}^{-1}$ . Thus the endothermic adsorption process has occured and it was in full agreement with the substantially higher protection efficiencies which have been observed as indicated in Figure $(1,2)$ .

The term b, defined by equation (6) is equilibrium constant of the adsorptiondesorption processes for methyl-urea-carbon steel system which may be represented as follows:

#### $\mathbf{b} = \exp(-\Delta \mathbf{G} \mathbf{a}/\mathbf{R} \mathbf{T})$  **=exp(Sa/R)exp(-Ha/RT) ……..(7)**

where  $\Delta Ga$ ,  $\Delta Sa$ ,  $\Delta Ha$  are respectively the changes in the free energy, entropy and enthalpy of adsorption of methyl urea on carbon steel specimen. Values of  $\Delta$ Ha in equation (7) may be considered to be those derived previously from the plots of Figure(4) using the values of b and  $\Delta$ Ha. It was possible to estimate the corresponding values of  $\Delta Sa$  and  $\Delta Ga$  at each of the four temperatures in the range (285-313)K and the resulting data are presented in Table (4). The negative value of  $\Delta G$  means that the adsorption of methyl urea extract on carbon steel surface is spontaneous process, and furthermore the negative values of  $\Delta G$  also show the strong interaction of inhibitor molecule into carbon steel surface[7].

The average values of  $\Delta Ga$  were obtained from the two methods are  $(-16.907, -15.036 \text{ kJ} \cdot \text{mol}^{-1})$ . These results indicate that methyl urea adsorption on the carbon steel specimen becomes more favourable with the rise of temperature for (285-313)K. This may account for the higher protection efficiencies of methyl urea over such temperatures. The value of  $\Delta S$ gives relatively greater degrees of freedom for the adsorbed molecules in the surface with a consequent enhancement in the rate of methyl urea adsorption.

This means the formation of an ordered stable layer of inhibitor on the carbon steel surface.

## **Kinetic Aspects**

 The rate (R) of corrosion of carbon steel in 1M HCl solution in the absence and the presence of methyl urea, increased with temperature over the range 285-313K. This is reflected in the variation of (log R) values, for both the blank (absence of methyl urea) and various solutions of methyl urea, with the reciprocal of temperature (1/T) in the manner depicted in Figure(5). The linear relationship observed between the values of (log R) and  $(1/T)$  Figure(5) confirms the Arrhenius type equation [11] :  $R = A exp(-E/RT)$ 

Where E is the apparent energy of activation for the corrosion process and A is the pre-exponetial factor. Values of E could thus be derived from the slopes of Figure $(5)$ . Fig. $(6)$  shows the resulting values of Ea as a function of methyl urea concentration in 1M HCl solution.

There was initial sharp decreases in Ea values (Figure.(6)) at methyl urea concentration  $1\times10^{-3}$ mM. Increasing of Ea values therafter steadily started with increasing methyl urea concentration to  $7.5 \times 10^{-2}$  mM. Thus, the presence of methyl urea in the acid medium probably alters the energy barrier for the metal corrosion through enhancing the apparent energy of activation resulting in the consequent decrease of the surface tendency for corrosion.

Table (5) shows the energy of activation Ea for the corrosion process and the per-exponential factor A.

A linear relationship was found to exist between the experimental values of log A and the corresponding values of Ea in Figure (7), which could be expressed as [15]:

## **Log A = (I + m Ea) ………….(9)**

where m and I are respectively the slope and the intercept of the plots in Fig.(7). Such a relationship is termed a (compensation effect) which is frequently found to describe the kinetics of catalytic reactions on alloys [16].

Equation (9) shows that simultaneous increase or decreases in Ea and log A for a particular system tend to compensate from the standpoint of the reaction rate.

## **Discussion**

 The most common and important electrochemical reactions in the corrosion of iron in the acidic solution is described by the following equations:

 $Fe + 2H^+ \rightarrow Fe^{2+} + H_2$  $Fe \rightarrow Fe^{2+} + 2e$  Anodic reaction (corrosion)  $2H^+ + 2e \rightarrow H_2$  Cathodic reaction (simplified)

Many organic inhibitors work by an adsorption mechanism. The resultant film of chemisorbed inhibitor is then responsible for protection either by physically blocking the surface from the corrosion environment or by retarding the electrochemical processes. The main functional groups capable of forming chemisorbed bonds with metal surfaces are amino  $[17]$  (-NH<sub>2</sub>), carboxyl (-COOH), and phosphonate  $(-PO_3H_2)$ although other functional groups or atoms can form co-ordinate bonds with metal surfaces. The protective properties of such compounds depend on the electron densities around the adsorption center. The higher electron density at the center, the more effective the inhibitor. The corrosion rate values (at low temperatures) in the presence of 1mm of methyl urea in acidic medium cause to increase the active sites on the metal surface by reducing the activation energy of rate determining step (rds) of the anodic or cathodic corrosion reaction.

The reduction in the dissolution of metal in the presence of methyl urea may be attributed to nitrogen and oxygen atoms present in the functional group. These groups are electroactive





# **Table (2): Protection efficiency, the degree of coverage at different temperature**

1/T	$b \times 10^3$		Log b			
$\times 10^{-3}$	loss	A.A	loss	A.A		
3.5	0.3937	0.3968	2.595	2.590		
3.44	0.6329	0.4545	2.8	2.658		
3.26	0.100	0.500	3	2.699		
31.9	0.9643	0.5181	2.98	2.714		

**Table (3): Maximum adsorption at different temperature** 

Table (4): Thermodynamic parameter  $\Delta G_a$ ,  $\Delta S_a$  and  $\Delta H_a$  of the adsorption **of methyl urea on carbon steel at different temperature** 

T(K)	$-\Delta G_a$ kJ.mol <sup>-1</sup> .K <sup>-1</sup>		$\Delta S_a$ J.mol <sup>-1</sup> .K <sup>-1</sup>		$\Delta H_a$ kJ.mol <sup>-1</sup> .K <sup>-1</sup>		
	loss	A.A loss		A.A	loss	A.A	
285	15.031	13.75	134.00	92.073	23.159	12.472	
291	15.835	14.30	134.00	92.073	23.159	12.472	
307	17.979	15.77	134.00	92.073	23.159	12.472	
313	18.783	16.324	134.00	92.073	23.159	12.472	

**Table (5): The energy of activation Ea for the corrosion** 

$\mathbf C$	Ea(kJ)		Log A				M	
Mm	Loss	A.A	loss	A.A	loss	A.A	loss	A.A
$\theta$	52.489	50.105	7.026	6.652	$-3.024$	$-1.7029$	0.1901	0.16304
50	50.893	48.929	6.577	6.321	$-3.024$	$-1.7029$	0.1901	0.16304
25	38.42	40.694	4.77	4.934	$-3.024$	$-1.7029$	0.1901	0.16304
10	41.327	47.752	3.839	5.98	$-3.024$	$-1.7029$	0.1901	0.16304
7.5	41.644	56.919	5.206	7.545	$-3.024$	$-1.7029$	0.1901	0.16304
5	35.914	54.782	4.2999	7.72	$-3.024$	$-1.7029$	0.1901	0.16304
	42.954	42.427	4.584	5.155	$-3.024$	$-1.7029$	0.1901	0.16304

 **process and the per-exponential factor A** 





**(b)** 



**(a) by using weight loss measurement. (b) by using atomic absorption measurement.** 



**(b)**<br>**Figure(3):** Langmuir adsorption of methyl urea **on carbon steel in 1M HCl plotted (C/) versus methyl urea concentration.** 

**(a) by using weight loss measurement. (b) by using atomic absorption** 

**measurement.** 





Figure (2): P% against methyl urea concentration at **temperature ranges (285-313)K. (a) by using weight loss measurement.** 

**(b) by using atomic absorption measurement.** 



- **Figure(4): Log b revsus (1/T)** 
	- **(a) by using weight loss measurement.** 
		- **(b) by using atomic absorption measurement.**





 **(b)** 

- **Figure (5): Arrhenius plot for the corrosion of carbon steel in 1M HCl at versus concentration.** 
	- **(a) by using weight loss measurement. (b) by using atomic absorption**
	-



**Figure.6: Values of apparent energy of activation**  $(E_a)$  for the corrosion of **carbon steel in 1M HCl solution as a function of methyl urea concentration (C/M)** 





**(b)** 

- **Figure (7): Ea values plotted versus log A for the corrosion of carbon steel in 1M**  with different urea **concentration.** 
	- **measurement. (a) by using weight loss measurement.**
	- **(b) by using atomic absorption**  (b) by using

and interact with the metals surface to a greater extent. Adsorption can be electrostatic or chemisorptive or the inhibitor can act simply by physically blocking the active sites.

The values of thermodynamic parameters for the adsorption of inhibitors can provide valuable information about the mechanism of corrosion inhibition. The endothermic adsorption process  $(\Delta H_a > 0)$  is attributed unequivocally to chemisorption [18], while generally, an exothermic adsorption process ( $\Delta H_a < 0$ ) may involve either physisorption or chemisorption or a mixture of both the processes. In the present case, the positive sign of  $\Delta H_a$  indicates that the adsoption of inhibitor molecules is an endothermic process[18]. The positive values of  $\Delta S$  indicate that the adsorption is a process accompanied by an increase in entropy. Therefore, the values of  $\Delta H$  and  $\Delta S_a$  obtained by both are in good agreement. The values of  $\Delta G_a$ are negative indicating that natural substance is strongly adsorbed at the metal surface[18]. A linear relationship between  $(C/\theta)$  and C suggests that the inhibitor undergoes adsorption according to the langmuir adsorption isotherm.

The temperature effect was significant in the presence of high concentration of methyl urea, and the P% increased with temperature increase generally. This results may be related to the modification of metal dissolution mechanism interpreted by many authors[16] . Temperature is a predominant factor in the formation of a protective layer at the metallic surface formed by metal inhibitor interaction, based on this reason.

### **References**

- 1. Rudresh, H.B. and Mayana S.M., **1977**, *"ndecylamine as a corrosion inhibitor for zinc in acidic solution"*, Br. Corros. J., 12, 1, 54- 56.
- 2. Schmitt, G., **1984**, *"Application of inhibitors for acid media"*, Br. Corros. J., 19, 4, 165- 176.
- 3. Abo El-Khair, B. Mostafa, **1984,** *"The effect of poly functional group compounds on the acid corrosion"*, Corrosion Prevention & Control, October, pp.17-19.
- 4. Thomas, J.G.M., Proc. Symp. On **1979**, *"Practical aspects of corrosion inhibition"*, Teddington, Februray, National Physical Laboratory.
- 5. Zor, S., **2002**, *"The effects of Benzoic acid in chloride solution on the corrosion of Iron*

*and Aluminum"*, Turk. J. Chem., 26, 403- 408.

- 6. Khalafalla, S.E., Shams El-Din, A.M. and Marci, S. A., **1959**, Rec. Trav. Chim. (from chemical abstract), 78, 513-518.
- 7. Saleh, Jalal M., Al-Saadie, Kh. A. S. and Hikmat, N. A., **1995,** *"Inhibtion effect of thiourea on the corrosion of low carbon steel in sulphuric acid",* Iraqi. J. Sci., 36, 3, 803-824.
- 8. Checmanowski, J. G., Gluszek, J., Masalski, J., **2003,** *"The effect of sequence of sol-gel multilayer coatings deposition on corrosion*  behaviour of stanless steel" 316L<sup>n</sup>, 21, 4, 387-396.
- 9. Ein-Eli, Y., **2004,** *"Enhanced corrosion inhibition of zinc"* Electrochemical and solid-state letters, 7, 1, 1-3.
- 10. Al-Mammar, D. E., **2002,** *"Using phosphate salts as inhibitors for corrosion of carbon steel in tap water"*, Iraqi J. Chem. 28, 2, 25- 34.
- 11. Fouda, A.S., El Desoky, A.M. and El Serawy, A.A. **2005,** *"Some hydrazide derivatives as inhibitors for the corrosion of zinc in sodium hydroxide solution"* The Journal of Corrosion Science and Engineering, 7, 1-12.
- 12. Al-Saadi, Kh. A. S., Al-Rufuie, E.A. and Al-Kubaisy, Shafia, **2002,** *"Inhibiting effect of diethyl amine on the corrosion of carbon steel in 1M hydrochloric acid"*, Iraqi Journal of Chemistry, 28, 1, 1-14.
- 13. Sekine, I., Okano, C. and Yuasa, M., **1990,** *"The corrosion behaviour of ferritic stainless steel in oxalic acid solutions",* Corrosion Science, 30, 4/5, 351-366.
- 14. Al-Saddi, Kh. A.S., **1997,** Ph.D., Thesis, College of Science, University of Baghdad.
- 15. Saleh, Jalal. M., **(1980)**, *"Surface chemistry and catalysis"*, College of Science, Baghdad University.
- 16. Isa, S. A. and Saleh M., **1972,** *"Surface chemistry and catalysis"*, J. Phs. Chem., 76, 2530-2539.
- 17. Schmitt, G., **1984,** *"Application of Inhibitor for acid media"*, Br. Corros. J., 19, 4, 165- 176.
- 18. Bouklah, M., Hammouti, B., **2006,** *"Thermodynamic characterization of steel corrosion for the corrosion inhibition of steel in sulphuric acid solutions by Artemisia",* Portugaliae Electrochimical Acta, 24, 457-468.

T °C	TK	1/T $\times 10^{-3}$	Con. mm	$\Delta \mathbf{wt}_{loss}$	Rateloss $mg.cm-2$ . $hour-1$	-log Rate	$\Delta$ wt <b>Atomic</b>	<b>Rate Atomic</b> $mg.cm-2$ . $hour-1$	-log Rate
12	285	3.5	$\boldsymbol{0}$	0.096	0.00355	2.4498	0.1200	0.00446	2.35066
18	291	3.44	$\boldsymbol{0}$	0.0057	0.00285	2.5452	0.0064	0.0032	2.4949
34	307	3.26	$\boldsymbol{0}$	0.0233	0.01165	1.9337	0.03	0.015	1.8239
40	313	3.19	$\boldsymbol{0}$	0.0424	0.01185	1.9263	0.044	0.022	1.6576
12	285	3.5	0.05	0.0569	0.00211	2.664	0.07944	0.00294	2.5317
18	291	3.44	0.05	0.0044	0.0022	2.658	0.00512	0.002559	2.5919
34	307	3.26	0.05	0.0184	0.0092	2.0362	0.02457	0.01228	1.9108
40	313	3.19	0.05	0.02372	0.01185	1.9263	0.029775	0.014887	1.8272
12	285	3.5	0.025	0.003	0.002	2.6989	0.07225	0.00268	2.5719
18	291	3.44	0.025	0.3078	0.00205	2.6882	0.00237	0.00474	2.3242
34	307	3.26	0.025	0.00455	0.00393	2.4056	0.024885	0.01244	1.9052
40	313	3.19	0.025	0.0152	0.01013	1.9944	0.02366	0.01183	1.92702
12	285	3.5	0.01	0.04706	0.001743	2.759	0.06021	0.00223	2.6517
18	291	3.44	0.01	0.00257	0.0012825	2.8919	0.00327	0.00163	2.7878
34	307	3.26	0.01	0.01631	0.008155	2.08857	0.0231	0.01155	1.9374
40	313	3.19	0.01	0.012	0.00655	2.1837	0.01578	0.00789	2.1029
12	285	3.5	0.0075	0.002	0.0013	2.886	0.0494	0.00183	2.7375
18	291	3.44	0.0075	0.00315	0.00175	2.75696	0.002514	0.00126	2.6300
34	307	3.26	0.0075	0.0111	0.007655	2.1161	0.0224	0.0112	1.9508
40	313	3.19	0.0075	0.0102	0.0068	2.16749	0.0180	0.009	2.0458
12	285	3.5	0.005	0.04984	0.001824	2.73904	0.0646	0.00239	2.6216
18	291	3.44	0.005	0.00281	0.001405	2.8523	0.00325	0.00163	2.7878
34	307	3.26	0.005	0.01724	0.008621	2.0644	0.0246	0.0122	1.9136
40	313	3.19	0.005	0.0131	0.00655	2.18376	0.02292	0.01146	1.9408
12	285	3.5	0.001	0.0714	0.00264	2.57859	0.0937	0.00347	2.4590
18	291	3.44	0.001	0.0033	0.00165	2.78252	0.003964	0.00198	2.7033
34	307	3.26	0.001	0.0217	0.00868	2.06148	0.0274	0.0137	1.8633
40	313	3.19	0.001	0.0249	0.01245	1.9048	0.01835	0.009178	2.0373

**Table (1): Corrosion rate (g/min) at different temperatures using different methyl urea concentration**