



UNSTEADY FREE CONVECTION FLOW OF THIRD GRAD ELECTRICALLY CONDUCTING FLUID PAST AN INFINITE VERTICAL PLATE

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Abstract

In this paper the problem of, unsteady, hydromagnetic free convective flow of viscous incompressible and electrically conducting third order fluids past in infinite vertical Porous plate in the presence of constant suction and heat absorbing sinks is considered. It is found that the velocity and temperature distribution equations are controlled by different dimensionless parameters, namely, Grashof number Gr , prandtl number pr , Eckert number Ec , sink strength s , material moduli β and coecostic parameter α . An analytic solution for each of the velocity and the temperature distribution is obtained. The velocity and temperature distributions are shown graphically taking many cases of Gr , pr , Ec , s , β and α .

,s β ,Gr , pr ,Ec

. α

Introduction

The problem of free convection flow of an electrically conducting third order fluid past a vertical plate under the influence of a magnetic field attracted many scientists, in view of its application in astrophysics, geophysics, engineering and aerodynamics...etc.

The unsteady free convection flow past an infinite plate with constant suction and heat

sources has been studied by Pop and Soundalgekar (1975) [1]. The effect of magnetic field on the convective flow of electrically conducting fluid past a semi-infinite flat plate has been analyzed by Gupta (1961) [2], Nanda and Mohanty (1970) [3]. Sacheti, Chardran and

Singh (1994) [1] have obtained an exact solution for the unsteady MHD problem Sahoo, Datta

and Biswal (2003) [2] have been studied the heat transfer in mercury (pr=0.02) and electrolytic solution (pr=1.0) past an infinite porous plate with constant suction in the presence of uniform magnetic field and heat sink.

Sharma et al. (2004) [3] has been studied unsteady MHD flow and heat transfer over continuous porous moving horizontal surface in the presence of an oscillating free stream and heat Source-Noushima et-al (2004) [4] had extended the above problem to viscoelastic fluid. Mostafa, Rafiuddin and Ramaria (2004) [5] have been studied unsteady MHD to extend the work of (Noushima et-al) with variable suction.

Finally, in this paper we will study unsteady free convection flow of third grade electrically conducting fluid, an analytic solution for each of the velocity and temperature distribution are obtained.

The governing equation

The Cauchy stress tensor T of a third grade fluid is defined by the Rivlin-Ericksen constitutive equation (Rivlin and Ericksen (1960) [6])

$$T = -pI + \mu A_1 + \alpha_1 A_2 + \alpha_2 A_1^2 + B_3 (tr A_1^2) A_1$$

Where:

P is pressure, I is the identity tensor, μ is coefficient of shear viscosity, while α_1, α_2 and β_r are the material constants which are satisfy $\mu \geq 0, \alpha_j \geq 0, \beta_r \geq 0$ and $\alpha_1 + \alpha_2 = 0$.

A_1 and A_2 are the first and second Rivlin-Ericksen tensors defined as

$$A_1 = \nabla V + \nabla V^T$$

$$A_2 = \frac{\partial A_1}{\partial t} + V \cdot \nabla A_1 + A_1 \nabla V + \nabla V^T A_1$$

Where: V is the velocity vector.

Let the x-axis be taken in the vertically upward direction along the infinite vertical plate and y-axis normal to it, neglecting the induced magnetic field and applying Boussinesq's approximation, In this case the continuity equation is:

$$\frac{\partial v^*}{\partial y^*} = 0 \tag{1}$$

$$v^* = -v_0 \text{ (constant)} \tag{2}$$

The momentum equation is:

$$\rho \left(\frac{\partial u^*}{\partial t^*} + v^* \frac{\partial u^*}{\partial y^*} \right) = \mu \frac{\partial^2 u^*}{\partial y^{*2}} + \alpha_1 \left(\frac{\partial^3 u^*}{\partial y^{*2} \partial t^*} + v^* \frac{\partial^3 v^*}{\partial y^{*2}} \right) + 6\beta_3 \left(\frac{\partial u^*}{\partial y^*} \right)^2 \frac{\partial^2 u^*}{\partial y^{*2}} + \rho_g \beta_g (T^* - T_0) \tag{3}$$

An the energy equation

$$\frac{\partial \theta^*}{\partial t^*} + v^* \frac{\partial \theta^*}{\partial y^*} = k \frac{\partial^2 \theta^*}{\partial y^{*2}} + s^* (\theta^* - \theta_\infty^*) + \frac{v}{c_p} \left(\frac{\partial u^*}{\partial y^*} \right)^2 \tag{4}$$

The associated boundary condition, of the problems are

$$u^* = 0, \theta^* = 1 \text{ at } y^* = 0 \tag{5-a}$$

$$u^* \rightarrow 0, \theta^* \rightarrow 1 \text{ at } y^* \rightarrow \infty \tag{5-b}$$

Method of Solution

To write the governing equation in dimensionless form, we introduce the following dimensionless quantities:

$$y = \frac{v_0 y^*}{v}, t = \frac{v_0^2 t^*}{v}, u = \frac{u^*}{v_0}, Gr = \frac{v_g \beta_3 (\theta_w^* - \theta_\infty^*)}{v_0^2}, pr = \frac{v}{k}, Ec = \frac{v_0^2}{c_p (\theta_w^* - \theta_\infty^*)}, \theta = \frac{(\theta^* - \theta_\infty^*)}{(\theta_w^* - \theta_\infty^*)}, \alpha = \frac{\alpha_1 v_0^2}{v^2}, \beta = \frac{\beta_3 v_0^4}{v^3}, \rho = \frac{v}{\mu} \text{ and } s = \frac{s^* v}{v_0^2} \tag{6}$$

Where pr, Gr, s and Ec are the prandtl number, Grashof number, sink strength and Eckert number respectively.

In the view of eqs (5) and (6), the governing equations (3) and eqs (4) can be written in dimensionless form as

$$\frac{\partial u}{\partial t} - \frac{\partial u}{\partial y} = \frac{\partial^2 u}{\partial y^2} + \alpha \left(\frac{\partial^3 u}{\partial y^2 \partial t} - \frac{\partial^3 u}{\partial y^3} \right) + \tag{7}$$

$$6\beta \left(\frac{\partial u}{\partial y} \right)^2 \left(\frac{\partial^2 u}{\partial y^2} \right) + Gr \theta$$

$$pr \frac{\partial \theta}{\partial t} - pr \frac{\partial \theta}{\partial y} = \frac{\partial^2 \theta}{\partial y^2} + pr s \theta + pr E \left(\frac{\partial u}{\partial y} \right)^2 \tag{8}$$

The corresponding boundary conditions, in non-dimensional form, are:

$$u = 0, \theta = 1 \text{ at } y = 0 \tag{9-a}$$

and

$$u \rightarrow 0, \theta \rightarrow 1 \text{ as } y \rightarrow \infty \quad (9-b)$$

To solve eqs (9) and (10), we assume

$$u(y,t) = u_0(y) + \epsilon e^{i\omega t} u_1(y) \quad (10-a)$$

and

$$\theta(y,t) = \theta_0(y) + \epsilon e^{i\omega t} \theta_1(y) \quad (10-b)$$

The substituting of eq (10.a,b) into equations (9) and (10) and equating the coefficients of ϵ , gives:

zero order equation

$$-u_0' = u_0'' + Gr \theta_0 - \alpha u_0''' + 6\beta u_0'' u_0'^2 \quad (11)$$

$$-pr \theta_0' = \theta_0' + pr s \theta_0 + pr Ec u_0'^2 \quad (12)$$

(12)

first order equation

$$i\omega u_1 - u_1' = u_1'' + Gr \theta_1 + \alpha i\omega u_1'' - \alpha u_1''' + 6\beta(u_0'^2 u_1'' + 2u_0'' u_0' u_1') \quad (13)$$

$$pr i\omega \theta_1 - pr \theta_1' = \theta_1'' + pr s \theta_1 + 2pr Ec u_0' u_1' \quad (14)$$

and the boundary conditions are :

$$u_0 = 0, u_1 = 0, \theta_0 = 1, \theta_1 = 0 \text{ at } y \rightarrow 0$$

$$u_0 \rightarrow 0, u_1 \rightarrow 0, \theta_0 \rightarrow 0, \theta_1 \rightarrow 0 \text{ at } y \rightarrow \infty$$

Equations(11-14) are nonlinear third order we are using multiparameters perturbation technique and assuming Ec is very small, therefore u, u_1, θ, θ_1 can be expanded in term of Ec , as follows:

$$\left. \begin{aligned} u_0 &= u_{01} + Ec u_{02}, & u_1 &= u_{11} + Ec u_{12} \\ \theta_0 &= \theta_{01} + Ec \theta_{02}, & \theta_1 &= \theta_{11} + Ec \theta_{12} \end{aligned} \right\} (15)$$

Putting the last equation into equations (11-14) and equating the power of Ec , we obtain

Zero order of Ec

$$-pr \theta_{01}' = \theta_{01}'' + pr s \theta_{01} \quad (16)$$

$$-pr \theta_{02}' = \theta_{02}'' + pr s \theta_{02} + pr u_{01}'^2 \quad (17)$$

$$-u_{01}' = u_{01}'' + Gr \theta_{01} - \alpha u_{01}''' + 6B u_{01}'' u_{01}'^2 \quad (18)$$

$$-u_{02}' = u_{02}'' + Gr \theta_{02} - \alpha u_{02}''' + 6B(u_{02}'' u_{01}'^2 + 2u_{01}'' u_{01}' u_{02}') \quad (19)$$

$$6B(u_{02}'' u_{01}'^2 + 2u_{01}'' u_{01}' u_{02}')$$

First order of Ec

$$pr i\omega \theta_{11} - pr \theta_{11}' = \theta_{11}'' + pr s \theta_{11} \quad (20)$$

$$pr i\omega \theta_{12} - pr \theta_{12}' = \theta_{12}'' + pr s \theta_{12} + 2pr u_{01}' u_{11}' \quad (21)$$

$$i\omega u_{11} - u_{11}' = u_{11}'' + Gr \theta_{11} + \alpha i\omega u_{11}'' - \alpha u_{11}''' + 6B(u_{01}'^2 u_{11}'' + 2u_{01}'' u_{01}' u_{11}') \quad (22)$$

$$i\omega u_{12} - u_{12}' = u_{12}'' + Gr \theta_{12} + \alpha i\omega u_{12}'' - \alpha u_{12}''' + 6B(u_{01}'^2 u_{12}'' + 2u_{01}'' u_{01}' u_{12}') + 2u_{01}'' u_{01}' u_{12}' + u_{02}'' u_{01}' u_{11}' + u_{02}' u_{01}'' u_{11}' \quad (23)$$

For small value of β , we can write

$$\left. \begin{aligned} \theta_{01} &= \theta_{011} + \beta \theta_{012}, & \theta_{02} &= \theta_{021} + \beta \theta_{022} \\ u_{01} &= u_{011} + \beta u_{012}, & u_{02} &= u_{021} + \beta u_{022} \\ \theta_{11} &= \theta_{111} + \beta \theta_{112}, & \theta_{12} &= \theta_{121} + \beta \theta_{122} \\ u_{11} &= u_{111} + \beta u_{112}, & u_{12} &= u_{121} + \beta u_{122} \end{aligned} \right\} (24)$$

From equations (16-23), we get Zero order of B

$$-pr \theta_{011}' = \theta_{011}'' + pr s \theta_{011} \quad (25)$$

$$-pr \theta_{012}' = \theta_{012}'' + pr s \theta_{012} \quad (26)$$

$$-pr \theta_{021}' = \theta_{021}'' + pr s \theta_{021} + pr u_{011}'^2 \quad (27)$$

$$-pr \theta_{022}' = \theta_{022}'' + pr s \theta_{022} + 2pr u_{011}' u_{012}' \quad (28)$$

(28)

$$-u_{011}' = u_{011}'' + Gr \theta_{011} - \alpha u_{011}''' \quad (29)$$

$$-u_{012}' = u_{012}'' - \alpha u_{012}''' + Gr \theta_{012} + 6(u_{011}'' u_{011}'^2)$$

$$(30)$$

$$-u_{021}' = u_{021}'' + Gr \theta_{021} - \alpha u_{021}''' \quad (31)$$

$$-u_{022}' = u_{022}'' + Gr \theta_{022} - \alpha u_{022}''' + 6(u_{021}'' u_{011}'^2 + 2u_{011}'' u_{011}' u_{021}') \quad (32)$$

$$(32)$$

First order of β

$$pr i\omega \theta_{111} - pr \theta_{111}' = \theta_{111}'' + pr s \theta_{111} \quad (33)$$

$$pr i\omega \theta_{112} - pr \theta_{112}' = \theta_{112}'' + pr s \theta_{112} \quad (34)$$

$$pr i\omega \theta_{121} - pr \theta_{121}' = \theta_{121}'' + pr s \theta_{121} + 2pr u_{011}' u_{111}' \quad (35)$$

$$pr i\omega \theta_{122} - pr \theta_{122}' = \theta_{122}'' + pr s \theta_{122} + 2pr(u_{011}' u_{112}' + u_{012}' u_{111}') \quad (36)$$

$$i\omega u_{111} - u'_{111} = u''_{111} + Gr\theta_{111} + \alpha i\omega u''_{111} - \alpha u'''_{111} \quad (37)$$

$$i\omega u_{112} - u'_{112} = u''_{112} + \alpha i\omega u''_{112} - \alpha u'''_{112} + 6(u''_{011} u'_{111} + 2u''_{011} u'_{011} u'_{111}) \quad (38)$$

$$i\omega u_{121} - u'_{121} = u''_{121} + Gr\theta_{121} + \alpha i\omega u''_{121} - \alpha u'''_{121} \quad (39)$$

$$i\omega u_{122} - u'_{122} = u''_{122} + Gr\theta_{122} + \alpha i\omega u''_{122} - \alpha u'''_{122} + 6(u''_{011} u'_{121} + 2u'_{011} u'_{021} u'_{111} + 2u''_{011} u'_{011} u'_{121} + u''_{021} u'_{011} u'_{111} + u'_{021} u''_{011} u'_{111}) \quad (40)$$

Finally if α is very small, we can write

$$\left. \begin{aligned} \theta_{011} &= q + \alpha q_0 & u_{011} &= w + \alpha v \\ \theta_{012} &= p + \alpha p_0 & u_{012} &= f + \alpha g \\ \theta_{021} &= q_1 + \alpha q_2 & u_{021} &= w_1 + \alpha v_1 \\ \theta_{022} &= p_1 + \alpha p_2 & u_{022} &= f_1 + \alpha g_1 \\ \theta_{111} &= q_3 + \alpha q_4 & u_{111} &= w_2 + \alpha v_2 \\ \theta_{112} &= p_3 + \alpha p_4 & u_{112} &= f_2 + \alpha g_2 \\ \theta_{121} &= q_5 + \alpha q_6 & u_{121} &= w_3 + \alpha v_3 \\ \theta_{122} &= p_5 + \alpha p_6 & u_{122} &= f_3 + \alpha g_3 \end{aligned} \right\} \quad (41)$$

And from equations (37-39), we get zero order of α

$$-prq = q'' + prsq \quad (42)$$

$$-prp = p'' + prsp \quad (43)$$

$$-prq_1 = q_1'' + prsq_1 + prw^2 \quad (44)$$

$$-w' = w'' + Grq \quad (45)$$

$$-f' = f'' + Grp + 6(w'' w^2) \quad (46)$$

$$-w_1' = w_1'' + Grq_1 \quad (47)$$

$$-prp_1 = p_1'' + prsp_1 + 2prw'f' \quad (48)$$

$$-f_1' = f_1'' + Grp_1 + 6(w_1'' w_1^2 + 2w'' w_1' w_1') \quad (49)$$

$$pri\omega q_3 - prq_3' = q_3'' + prsq_3 \quad (50)$$

$$pri\omega p_3 - prp_3' = p_3'' + prsp_3 \quad (51)$$

$$pri\omega q_5 - prq_5' = q_5'' + prsq_5 + 2prw'w_2' \quad (52)$$

$$pri\omega p_5 - prp_5' = p_5'' + prsp_5 + 2pr(w'f_2' + f'w_2') \quad (53)$$

$$i\omega w_2 - w_2' = w_2'' + Grq_3 \quad (54)$$

$$i\omega f_2 - f_2' = f_2'' + 6(w'' w_2^2 + 2w'' w_1' w_2') \quad (55)$$

$$i\omega w_3 - w_3' = w_3'' + Grq_5 \quad (56)$$

$$i\omega f_3 - f_3' = f_3'' + Grp_5 + 6[w'' w_3^2 + 2w_1' w_1' w_2'' + 2w'' w_1' w_3' + w_1'' w_1' w_2' + w_1' w'' w_2'] \quad (57)$$

First order of α

$$-prq_0 = q_0'' + prsq_0 \quad (58)$$

$$-prp_0 = p_0'' + prsp_0 \quad (59)$$

$$-prq_2 = q_2'' + prsq_2 + 2prw'v' \quad (60)$$

$$-prp_2 = p_2'' + prsp_2 + 2pr(w'g' + v'f') \quad (61)$$

$$-v' = v'' + Grq_0 - w''' \quad (62)$$

$$-g' = g'' - f''' + Grp_0 + 6[w'' v'' + 2w'v'w''] \quad (63)$$

$$-v_1' = v_1'' + Grq_2 - w_1''' \quad (64)$$

$$-g_1' = g_1'' + Grp_2 - f_1''' + 6[(w'' v_1'' + 2w_1'v_1'w_1'') + 2(w''w'v_1' + v''w'w_1' + v'w''w_1')] \quad (65)$$

$$pri\omega q_4 - prq_4' = q_4'' + prsq_4 \quad (66)$$

$$pri\omega p_4 - prp_4' = p_4'' + prsp_4 \quad (67)$$

$$pri\omega q_6 - prq_6' = q_6'' + prsq_6 + 2pr(w'v_2' + v'w_2') \quad (68)$$

$$pri\omega p_6 - prp_6' = p_6'' + prsp_6 + 2pr[w'g_2' + v'f_2' + f'v_2' + g'w_2'] \quad (69)$$

$$i\omega v_2 - v_2' = v_2'' + Gr q_4 + i\omega w_2'' - w_2''' \quad (V_0)$$

$$i\omega g_2 - g_2' = g_2'' + i\omega f_2'' - f_2''' + 6[w_2'^2 v_2'' + 2w_2' v_2' w_2'' + 2w_2'' w_2' v_2'] + v_2'' w_2' w_2'' + v_2' w_2'' w_2''' \quad (V_1)$$

$$i\omega v_3 - v_3' = v_3'' + Gr q_6 + i\omega w_3'' - w_3''' \quad (V_2)$$

$$i\omega g_3 - g_3' = g_3'' + Gr p_6 + i\omega f_3'' - f_3''' + 6[w_3'^2 v_3'' + 2w_3' v_3' w_3'' + 2(w_3' w_1' v_2'' + v_2' w_1' w_2'' + v_1' w_1' w_2'') + 2(w_3'' w_1' v_2' + v_2'' w_1' w_3' + v_1'' w_1' w_3' + w_1'' w_1' v_2' + v_1' w_1'' w_2' + w_1' w_1'' v_2') + v_2'' w_1' w_2' + v_1' w_1'' w_2''] \quad (V_3)$$

Solving these differential equations (V₀-V₃) with the aid of the corresponding boundary conditions and then substituting these solutions into relation (10, 11, 12), we obtain the velocity distribution u and temperature distribution θ as

$$u = \frac{A_1 Gr}{pr^{3/2}(-2 + pr + \sqrt{pr}\sqrt{pr-4s})^4} e^{-y} + \frac{4Gr\alpha}{\sqrt{pr}(\sqrt{pr} + \sqrt{pr-4s})} e^{-y} y + (A_2 Gr + \alpha Gr^3) + \beta \left(Gr^3 \alpha A_3 e^{-3y} + A_4 e^{\frac{1}{2}(4+pr-\sqrt{pr}\sqrt{pr-4s})y} + \frac{2}{3} Gr^2 \alpha (A_5 e^{\frac{1}{2}(-8+3pr+3\sqrt{pr}\sqrt{pr-4s})y} + \frac{A_6 e^{(-1-pr-\sqrt{pr}\sqrt{pr-4s})y}}{(-2 + pr + \sqrt{pr}\sqrt{pr-4s})^4 (pr + \sqrt{pr}\sqrt{pr-4s})^3} + (\frac{32pr^3 \sqrt{pr-4s}}{\sqrt{pr}(-2 + pr + \sqrt{pr}\sqrt{pr-4s})} + A_7) e^{-y} y^2) \right) + Ec \left(\left(A_8 e^{-y} y + A_9 e^{\frac{1}{2}(pr+\sqrt{pr}\sqrt{pr-4s})y} \right) + \alpha (A_{10} e^{-y} y^2) \right) + \beta \left(A_{11} e^{\frac{1}{2}(-4-pr+\sqrt{pr}\sqrt{pr-4s})y} + A_{12} e^{\frac{1}{2}(-2+pr+\sqrt{pr}\sqrt{pr-4s})y} + A_{13} e^{\frac{1}{2}(-12+7pr+7\sqrt{pr}\sqrt{pr-4s})y} \right) + e^{i\omega t}$$

$$\left\{ \frac{(2(e^{\frac{1}{2}(1+\sqrt{1+4i\omega})y} - e^{\frac{1}{2}\sqrt{pr}(\sqrt{pr}+\sqrt{pr-4s+4i\omega})y}))Gr)}{(pr^2 + pr(-1-2s+2i\omega) - \sqrt{pr}\sqrt{pr-4s+4i\omega} + pr^{3/2})} + \alpha (A_{14} e^{\frac{1}{2}(1+\sqrt{1+4i\omega})y} + A_{15} e^{-\frac{1}{2}\sqrt{pr}(\sqrt{pr}+\sqrt{pr-4s+4i\omega})y}) + \beta (A_{16} e^{\frac{1}{2}(5+\sqrt{1+4i\omega})y} + \alpha A_{17} e^{\frac{1}{2}(3-pr-\sqrt{pr-4s+\sqrt{1+4i\omega}})y} + (A_{18} + \alpha A_{19}) e^{\frac{1}{2}(-2-\sqrt{pr}(\sqrt{pr-4s+\sqrt{pr-4s+4i\omega}})y} + A_{20} e^{(-\frac{1}{2}(pr+\sqrt{pr}\sqrt{pr-4s})+\frac{1}{2}(-1-\sqrt{1+4i\omega}))y} + (A_{21} + \alpha A_{22}) e^{\frac{1}{2}(-2+\sqrt{pr}(\sqrt{pr-4s})-\sqrt{pr-4s+4i\omega})y} + (A_{23} + \alpha A_{24}) e^{\frac{1}{2}(-3+pr+(\sqrt{pr-4s+\sqrt{1+4i\omega}})y} + (A_{25} + \alpha A_{26}) e^{-\frac{1}{2}(1-2pr+2\sqrt{pr}\sqrt{pr-4s+\sqrt{1+4i\omega}})y} + Ec((A_{27} + \alpha A_{28}) e^{-\frac{1}{2}(1-pr-\sqrt{pr}\sqrt{pr-4s+\sqrt{1+4i\omega}})y} + (A_{29} + \alpha A_{30}) e^{-\frac{1}{2}(3+\sqrt{1+4i\omega})y} + A_{31} e^{-\frac{1}{2}(2+pr+\sqrt{pr}\sqrt{pr-4s+4i\omega})y}) + \eta \right\} \quad (V_4)$$

where $A_1, A_2, A_3, \dots, A_{31}$ and η is a function of $pr, Gr, \alpha, \beta, s, y, i, \omega$

And

$$\theta = e^{\frac{1}{2}(pr+\sqrt{pr}\sqrt{pr-4s})y} + Ec \left(\frac{-2 Gr pr^3 e^{-y}}{(pr^2 + pr^{3/2}\sqrt{pr-4s})(1 + pr(-1+s))} + \alpha \left(\frac{8192 Gr^2 pr^{19/2} \sqrt{pr-4s}}{((-1+pr)^4 (4-pr+\sqrt{pr}\sqrt{pr-4s})^2} + D_1 e^{\frac{1}{2}\sqrt{pr}(\sqrt{pr}+\sqrt{pr-4s})y} + \beta (D_2 e^{\frac{1}{2}(pr+\sqrt{pr}\sqrt{pr-4s})y} + D_3 e^{\frac{1}{2}(-6+pr+\sqrt{pr}\sqrt{pr-4s})y} + D_4 e^{-4y} + D_5 e^{\frac{1}{2}(-2+3pr+3\sqrt{pr}\sqrt{pr-4s})y} + \alpha (D_6 e^{\frac{1}{2}(-2+\sqrt{pr}\sqrt{pr-4s})y} + D_7 e^{\frac{1}{2}\sqrt{pr}(\sqrt{pr}+\sqrt{pr-4s})y} + \frac{1}{2}(2(-3+\frac{1}{2}(pr+\sqrt{pr}\sqrt{pr-4s})+\sqrt{pr}\sqrt{pr-4s})y} + D_8 e^{\frac{1}{2}\sqrt{pr}(\sqrt{pr}+\sqrt{pr-4s})y} + \frac{1}{2}(pr+2(-2+pr+\sqrt{pr}\sqrt{pr-4s})+\sqrt{pr-4s})y} \right) \right)$$

$$\begin{aligned}
 &+ D_9 e^{(-8+pr-4(-pr-\sqrt{pr}\sqrt{pr-4s})y+(5-pr+\frac{9}{2}(-pr-\sqrt{pr}\sqrt{pr-4s})y))} \\
 &+ \epsilon e^{-i\omega t} (D_{10} e^{\frac{1}{2}(pr+\sqrt{pr}\sqrt{pr-4s+4i\omega})} + Ec((\\
 &+ D_{11} e^{\frac{1}{2}(-pr-\sqrt{pr}\sqrt{pr-4s})y-\frac{1}{2}\sqrt{pr}\sqrt{pr+\sqrt{pr-4s+4i\omega})y} \\
 &+ \alpha(e^{\frac{1}{2}\sqrt{pr}(\sqrt{pr}+(\sqrt{pr-4s+4i\omega}))y} \\
 &+ D_{12} e^{\frac{1}{2}(-2pr+\sqrt{1+4i\omega}-\sqrt{pr}(\sqrt{pr-4s}+(\sqrt{pr-4s+4i\omega}))y} \\
 &+ D_{13} e^{\frac{1}{2}(1-2pr+\sqrt{1+4i\omega}-\sqrt{pr}(\sqrt{pr-4s}+(\sqrt{pr-4s+4i\omega}))y} \\
 &+ D_{14} e^{\frac{1}{2}(pr+\sqrt{pr}\sqrt{pr-4s+4i\omega}+2(-1+\frac{1}{2}(-pr-\sqrt{pr}\sqrt{pr-4s+4i\omega}))y} \\
 &+ D_{15} e^{\frac{1}{2}(1-2pr+\sqrt{1+4i\omega}-\sqrt{pr}(\sqrt{pr-4s}+(\sqrt{pr-4s+4i\omega}))y))}) + \psi
 \end{aligned} \tag{V0}$$

where D_1, D_2, \dots, D_{15} and ψ is a function of $pr, Gr, \alpha, \beta, s, \omega, y, i$

Skin Friction and Nusselt number

We can find the coefficient of Skin Friction by using the formula

$$\begin{aligned}
 C_p &= -\left(\frac{\partial u}{\partial y}\right)_{y \rightarrow 0} \\
 &= \frac{2Gr}{-pr - \sqrt{pr}\sqrt{pr-4s}} + \frac{2Gr\alpha}{(\sqrt{pr}(\sqrt{pr} + \sqrt{pr-4s}))} \\
 &\frac{(-2 - pr - \sqrt{pr}\sqrt{pr-4s}(-pr^2 - pr^{3/2}\sqrt{pr-4s}))}{(-2 + pr + \sqrt{pr}\sqrt{pr-4s})^2} \\
 &\frac{4Gr\alpha(-2 + pr + pr(pr + \sqrt{pr}\sqrt{pr-4s} - 2s))}{\sqrt{pr}(\sqrt{pr} + \sqrt{pr-4s})(-2 + pr + \sqrt{pr}\sqrt{pr-4s})^2} + \\
 &\beta \frac{4Gr^3}{(-2 + pr + \sqrt{pr}\sqrt{pr-4s})^3} (24\sqrt{pr}(\sqrt{pr-4s}) \\
 &(-1 - pr - \sqrt{pr}\sqrt{pr-4s})(1 + pr + \sqrt{pr}\sqrt{pr-4s})^3 - \\
 &\frac{(6\sqrt{pr}(\sqrt{pr}\sqrt{pr-4s})(4 + pr + \sqrt{pr}\sqrt{pr-4s})^3)}{(2 + pr + \sqrt{pr}\sqrt{pr-4s})} \\
 &Ec(-4Gr^3(9pr^3(-1+s) + 9pr^{5/2}\sqrt{pr-4s}(-1+s) \\
 &- 40s + \sqrt{pr}(1 + pr(-1+s))(pr^{3/2}
 \end{aligned}$$

$$\begin{aligned}
 &+ pr\sqrt{pr-4s} - 3\sqrt{pr}s - \sqrt{pr-4s}) \\
 &- 9pr^2(-3 + s + 3s^2) + pr(-20 - 7s + 72s^2) + \\
 &2(\sqrt{pr}(10 - 23s)\sqrt{pr-4s} + 20s - pr^3(-5 + 5s) \\
 &+ \epsilon e^{-i\omega t} (\beta(6Gr^3((Gr(\sqrt{pr}\sqrt{pr-4s} + 4i\omega))^2 \\
 &\frac{1}{2}(pr + \sqrt{pr-4s} + 4i\omega)))/(2(pr(-1 - 2s + 2i\omega)) \\
 &- \sqrt{pr}\sqrt{pr-4s} + 4i\omega + pr^{3/2}) + \\
 &(2iGr(pr + \sqrt{pr}\sqrt{pr-4s} + 4i\omega))^2 + \\
 &i\omega\omega)/(pr^2 - \sqrt{pr}\sqrt{pr-4s} + 4i\omega + \\
 &pr^{3/2}\sqrt{pr-4s} + 4i\omega - 2i\omega)) / \\
 &((-1 + \frac{1}{2}(-\sqrt{pr}\sqrt{pr-4s}))^2 \\
 &+(pr + \sqrt{pr}\sqrt{pr-4s} + 4i\omega)^2 - i\omega)(1 + 4i\omega) \\
 &+ pr(10 + 5s - 36s^2) + \sqrt{pr-4s}(-14 + 5s^2) \\
 &+ pr^2(-14 + 3s + 15s^2)))) / \\
 &(\sqrt{pr}(\sqrt{pr} + \sqrt{pr-4s})^3(1 + pr(-1 + s)) \\
 &(40 + 9pr^3 + 9pr^{5/2}\sqrt{pr-4s} \\
 &- 9pr^{3/2}\sqrt{pr-4s}(2 + s)pr(-7 + 36s))) + \epsilon e^{i\omega t} (\\
 &(\beta(-Gr^3 pr^{12}s^3)/((-1 + \frac{1}{2}(-pr - \sqrt{pr}\sqrt{pr-4s})) \\
 &(pr + (-1 + \sqrt{1+4i\omega})(\sqrt{1+4i\omega} - \sqrt{pr-4s} + 4i\omega))^2 \\
 &(1 - 2pr - \sqrt{pr}\sqrt{pr-4s} + pr^{3/2}\sqrt{pr-4s} + 4i\omega))) + \\
 &\alpha \frac{(Gr^2 pr(pr + \sqrt{pr}\sqrt{pr-4s}))}{(pr^2 + pr^{3/2}\sqrt{pr-4s} + 4i\omega - 2i\omega)} \\
 &+ \frac{Gr pr((\sqrt{pr} + \sqrt{pr-4s} + 4i\omega) + i\omega)}{2(pr^2 + pr^{3/2}\sqrt{pr-4s} + 4i\omega - 2i\omega)})) + \zeta
 \end{aligned}$$

where ζ is a function of $pr, Gr, \alpha, \beta, s, \omega, y, i$. The rate of heat transfer in terms of Nusselt number at the plate is

$$\begin{aligned}
 Nu &= -\left(\frac{\partial \theta}{\partial y}\right)_{\theta \rightarrow 0} \\
 &= -\frac{1}{2}(-pr - \sqrt{pr}\sqrt{pr-4s}) + Ec(\\
 &(-1 + pr + \frac{1}{2}(4 - 3pr - 3\sqrt{pr}\sqrt{pr-4s}) \\
 &\frac{1}{2}(-pr - \sqrt{pr}\sqrt{pr-4s}) + \\
 &pr(+\frac{1}{2}(-3pr - 3\sqrt{pr}\sqrt{pr-4s}s))/(\sqrt{pr}\sqrt{pr-4s})
 \end{aligned}$$

$$\begin{aligned}
 & + \beta(-8192Gr^4 pr \frac{(-pr - \sqrt{pr}\sqrt{pr-4s})}{2pr(\sqrt{pr} + \sqrt{pr-4s})^4} + \\
 & \alpha(pr^4 \frac{6Gr^4}{((-1 + \frac{1}{2}(-pr - \sqrt{pr}\sqrt{pr-4s}))^5))}) \\
 & + \alpha(6Gr^3(1 + \sqrt{1+4i\omega}))/((-1 + \frac{1}{2}(-\sqrt{pr}\sqrt{pr-4s}))^2 \\
 & (pr^2 + (-2s + 2i\omega) + pr^{3/2}\sqrt{pr-4s+4i\omega} - 2i\omega)) \\
 & + (3Gr^3(\sqrt{1+4i\omega})^2)/((-1 + \frac{1}{2}(-pr - \sqrt{pr-4s}))^2 \\
 & (pr^2 + pr(-1 - 2s + 2i\omega) - \sqrt{pr}\sqrt{pr-4s})^2 - \\
 & \sqrt{pr}\sqrt{pr-4s+4i\omega} - 2i\omega)) + \varphi
 \end{aligned}$$

Where φ is a function of $pr, Gr, \alpha, \beta, s, \omega, y, i$

Results and discussions

In this section, we will study the effects of different dimensionless numbers upon velocity and temperature distribution.

Figures (1-6), illustrate the effect of each of material moduli, coecostic parameter, prandtl number, Grashof number, sink strength and Eckerts number, upon the velocity component respectively.

Figure (1) exhibit the effect of material moduli β upon the velocity component, the velocity increases as material moduli ($\beta = 0.0000, 0.1, 1.3, 2$) increase. Figures (7, 8) show the effects of the coecostic parameter upon the velocity component, we observe that there is small change in velocity values even for large value of α .

From figure (9), it is observed that the velocity is increases when there is increasing in Grashof number. However, figure (10), shows opposite effect with prandtl number. The sink strength has the same effects as Grashof number with some different in velocity values, see figure (11). The effect of dimensionless parameters upon temperature are shown in figures (12-17).

We note that there is increasing in temperature values as the material parameter β decreases, but this is true only for very small values of β , see figures (18, 19).

Figure (2, 3), shows the effect of coecostic parameter α upon the temperature, this effect is clear for large values of α . Prandtl number and Grashof number have opposite effects upon temperature distribution, see figures(4) and

(5). Figure (6) shows the effect of s upon the temperature distribution.

Table 1 shows that as material moduli β increase there is increasing in the value of the skin frication coefficient C_p , also as α increases there is a small increasing in the C_p value. Table 2 shows that as Gr or s increasing there is increasing in C_p . However, the increasing in prandtl number resulting a decreasing in C_p . Table 3 shows that as α or B increasing there is increasing in the Nusselte number Nu . Table 4 shows that as Gr increasing there is increasing in Nusselte number Nu , however as sink strength s or Prandtl number pr increase loads to a decreasing in Nusselte number Nu .

Velocity distribution

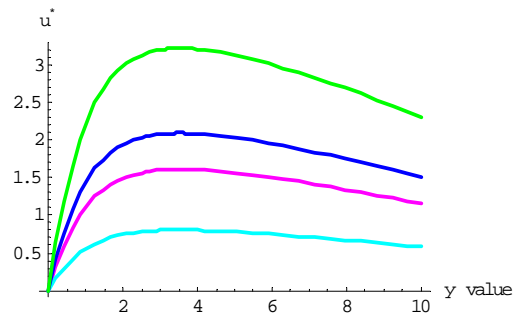


Figure 1: $Gr=0, Ec=0.001, \omega=0, pr=0.2, s=0.1, \alpha=0.1, t=Pi/10, \epsilon=0.2, \beta=0.0000, \beta=0.1, \beta=1.3, \beta=2$

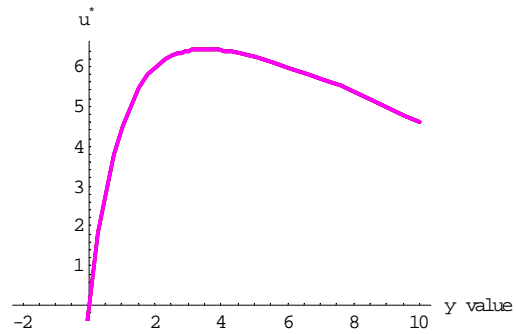


Figure 2: $Gr=0, Ec=0.001, \omega=0, p=0.2, S=0.1, \beta=0.1, t=Pi/10, \epsilon=0.2, \alpha=0.1, \alpha=0.001, \alpha=0.0001, \alpha=0.00001$

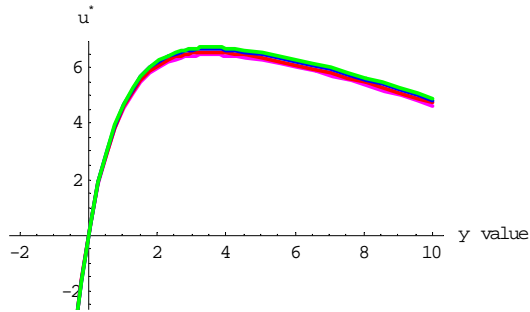


Figure 3: $Gr=0, Ec=1.1, \omega=0, pr=0.2, s=1.1, \beta=0.4, t=Pi/1.1, \epsilon=0.2$
 $\alpha=1, \alpha=1.1, \alpha=1.2, \alpha=1.3$

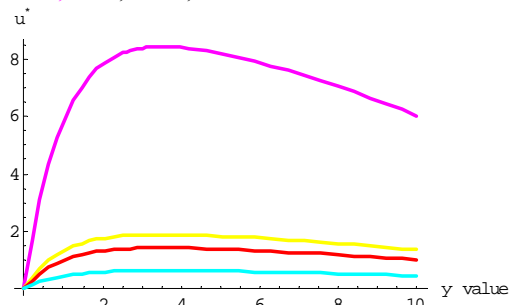


Figure 4: $Ec=1.1, \omega=0, pr=0.2, S=1.1, \alpha=1.1, \beta=0.4, t=Pi/1.1, \epsilon=0.2$
 $Gr=0, Gr=1.1, Gr=1.2, Gr=1.3$

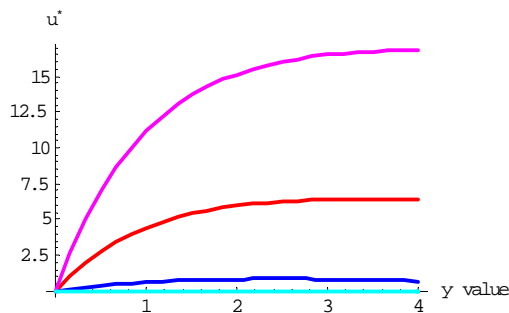


Figure 5: $Gr=0, Ec=1.1, \omega=0, s=1.1, \alpha=1.1, \beta=0.4, t=Pi/1.1, \epsilon=0.2$
 $Pr=0.1, pr=0.2, pr=0.3, pr=0.4$

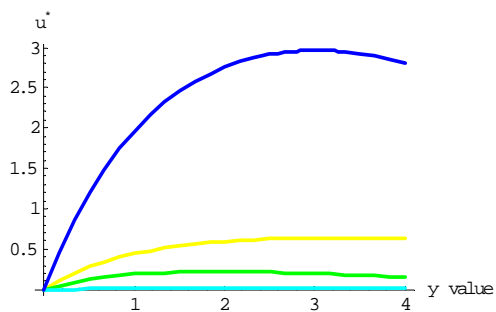


Figure 6: $Gr=0, Ec=1.1, \omega=0, pr=0.2, \alpha=1.1, \beta=0.4, t=Pi/1.1, \epsilon=0.2$
 $s=1.1, s=1.2, s=1.3, s=1.4$

Temperature distribution

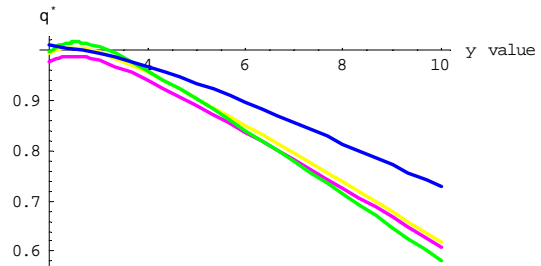


Figure 7: $Gr=0, Ec=1.1, \omega=0, pr=0.2, s=1.1, \alpha=1.1, t=Pi/1.1, \epsilon=0.2$
 $\beta=0.1, \beta=0.2, \beta=0.3, \beta=0.4$

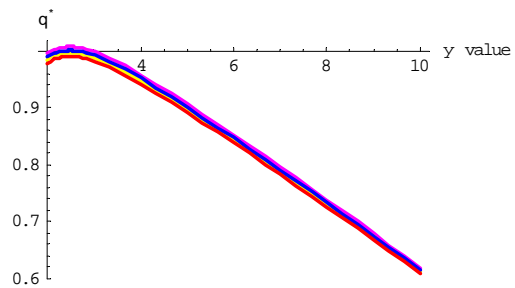


Figure 8: $Gr=0, Ec=1.1, \omega=0, pr=0.2, s=1.1, \alpha=1.1, t=Pi/1.1, \epsilon=0.2$
 $\beta=1, \beta=1.1, \beta=1.2, \beta=1.3$

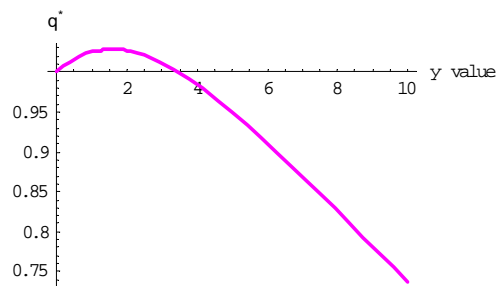


Figure 9: $Gr=0, Ec=1.1, \omega=0, pr=0.2, s=1.1, \beta=1.1, t=Pi/1.1, \epsilon=0.2$
 $\alpha=1.1, \alpha=1.2, \alpha=1.3, \alpha=1.4$

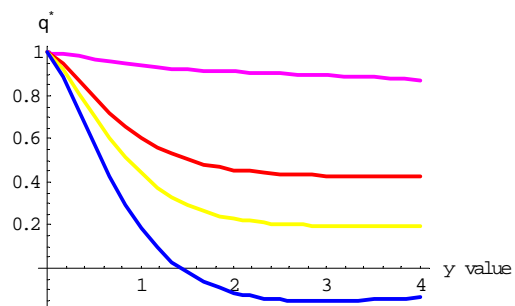


Figure 10: $Gr=0, Ec=1.1, \omega=0, pr=0.2$

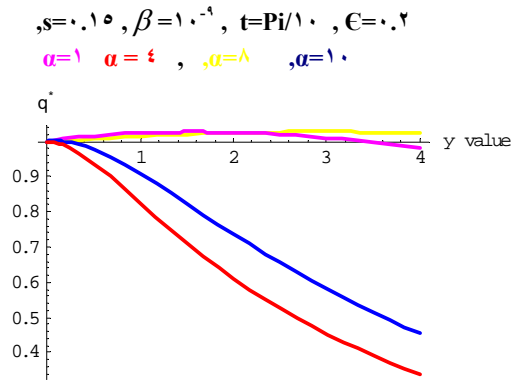


Figure 11: $\omega=0, Gr=0, Ec=0.001, \alpha=0.1$
 $\beta=10^{-4}, t=Pi/10, \epsilon=0.2,$
 $Pr=0.001, pr=0.020, pr=0.3, pr=0.5,$

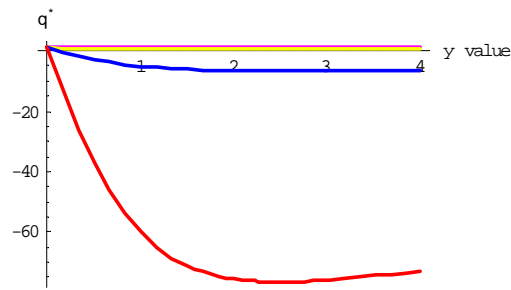


Figure 12: $Ec=0.001, \omega=0, pr=0.020,$
 $s=0.10,$
 $\alpha=0.1, \beta=10^{-4}, t=Pi/10, \epsilon=0.2$
 $Gr=0, Gr=10, Gr=100, Gr=200$

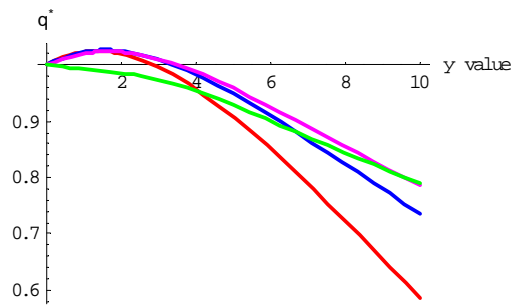


Figure 13: $Gr=0, Ec=0.001, \omega=0, pr=0.020,$
 $\alpha=0.1, \beta=10^{-4}, t=Pi/10, \epsilon=0.2$
 $S=0.0, s=0.3, s=0.10, s=0.1$

Table 1: Values of Sink Friction C_p when $t=Pi/10, \epsilon=0.2, Gr=0, Ec=0.001, \omega=0, pr=0.020, s=0.10.$

α	β	C_p
0.1	0.00005	0.177724
0.1	0.004	0.533171
0.1	0.3	0.710894
0.1	0.1	0.888718
0.1	1	1.77797
0.1	1.3	2.31137
0.1	1.8	3.20030
0.1	2	3.00090
0.00001	0.4	0.177732
0.0001	0.4	0.177730
0.001	0.4	0.177729
0.1	0.4	0.177728
1	0.4	0.306938
4	0.4	0.371416
8	0.4	0.376387
10	0.4	0.370372

Table 2: Values of Sink Friction C_p when $t=Pi/10, \epsilon=0.2, Ec=0.001, \omega=0, \alpha=0.1, \beta=0.4.$

Gr	pr	s	C_p
0	0.020	0.10	0.300471
10	0.020	0.10	0.460909
10	0.020	0.10	0.527899
20	0.020	0.10	0.710777
0	0.001	0.10	0.444783
0	0.020	0.10	0.300090
0	0.30	0.10	0.249078
0	0	0.10	0
0	0.020	0.02	0.117073
0	0.020	0.10	0.244070
0	0.020	0.10	0.300471
0	0.020	3	0.378472

0	0.20	0.10	4.2400
0	0.20	3	3.76438

Table ۳: Values of Rate of Heat Transfer (Nusselt number Nu) when $t=Pi/10$, $\epsilon=0.2$, $Gr=0$, $Ec=0.01$, $\omega=0$, $pr=0.20$, $s=0.10$.

α	β	Nu
0.1	0.0000000004	1.33310
0.1	0.000000003	1.09978
0.1	0.0000002	1.99973
0.1	0.0001	2.17730
0.1	1	2.00748
0.1	1.2	2.68967
0.1	1.6	4.02280
0.1	2	0.30603
0.00001	0.1	1.30230
0.00001	0.1	1.26940
0.001	0.1	1.26710
0.01	0.1	1.26007
1	0.1	1.18791
4	0.1	1.26141
8	0.1	2.02007
10	0.1	2.02777

Table 4: Values of Rate of Heat Transfer (Nusselt number Nu) when $t=Pi/10$, $\epsilon=0.2$, $Ec=0.01$, $\omega=0$, $a=0.1$, $\beta=10^{-1}$.

Gr	pr	s	Nu
0	0.20	0.10	1.30748
10	0.20	0.10	1.97101
100	0.20	0.10	2.79203
200	0.20	0.10	3.29947
0	0.01	0.10	4.28471
0	0.20	0.10	3.43803
0	0.30	0.10	3.37071
0	0	0.10	1.30702
0	0.20	0.2	4.70088
0	0.20	0.10	4.22298

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